



## Creating new CST markets through solar fuels

**ASTRI Symposium on The Future of Concentrating Solar Thermal Technology** 

Graham 'Gus' Nathan, Wojceich Lipinski, Jim Hinkley and the team

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### **Drivers for solar fuels**

#### **Electricity**

- Steam turbine
- Gas turbine
- Future cycles



Wholesale ~\$12/GJ

 $\eta_{heat-power} \sim 35\%$ 

"Non" Exportable

Growing role in light vehicle transport Possible role in heavy freight



Source: CSIRO.au

#### **Liquid transport fuels**

- Gasification: Biomass &/or coal
- Reforming: Natural gas
- Splitting: CO<sub>2</sub> & H<sub>2</sub>O



Wholesale ~ \$26/GJ

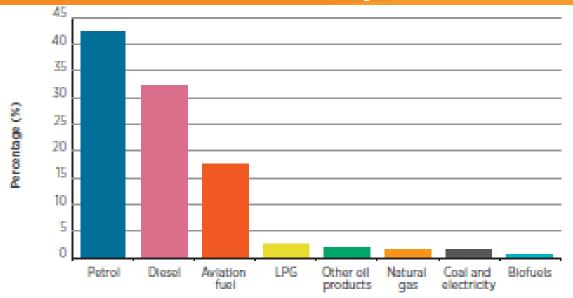
 $\eta_{heat\text{-fuel}} \sim \textbf{20-60}\%$ 

**Exportable commodity** 

Vital for heavy transport

**Essential for air transport** 

## Fractional demand for oil products



Share

72.8

19.1

3.3

3.3

1.5

100.0

(per cent)

2013-14

PJ

1156.9

303.0

52.0

53.0

24.3

1589.2

Average annua	l growth
2013–14 (per cent)	10 years (per cent)
-0.1	1.3
4.9	4.6
-	

Source: BREE (2014)

4.4 6.2 -2.5-3.4-0.11.1

Average

Source: Aus Energy Update (2015)

Total transport

Road

Rail

Water

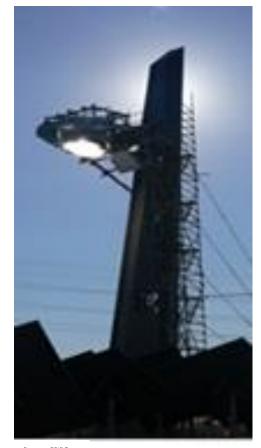
Other

## Comparing feed-stock and technologies

Feedstock	Efficiency solar to feed-stock	LHV feed- stock (MJ/kg)	Feed-stock present cost (\$/tonne)	Feed-stock future cost trend	Resource sustainable capacity	Comment
Oil-rich crops (Gen I)	~3%	~18	~ \$60	stable	zero	Unsustainable because it competes with food crops
Agricultural residues	~3%	~15	\$10-40	stable	Significant niche	CST ↑ output by ~30% - 40% from limited, valuable resource
Woody biomass (Gen II)	~3%	~15	\$150-\$250	stable	Significant niche	CST ↑ output by ~30% - 40% from limited additional resource
Macro & Micro algae (Gen III)	~20%	~15	\$180-450	down	Large (sea-water)	CST ↓ cost of more larger, more expensive, sustainable resource
CO <sub>2</sub> from flue- gas	-	0	~ \$60	down	Large	Challenging cost targets, but may be necessary
CO <sub>2</sub> from air	-	0	~ \$600	down	"Infinite"	Likely to be the most expensive of all CST options

## Targets and path to market

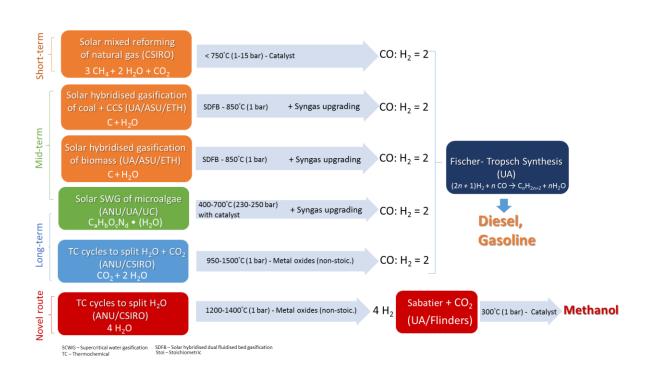
- Original targets for synthetic diesel by Fischer-Tropsch
  - \$1:20/L with 10% reduction in CO<sub>2</sub> re mineral crude
  - \$2:50/L with sustainable feed-stock and 50% reduction in CO<sub>2</sub>
- Path-way to market
  - Establish market with high value biomass co-products / fossil bends
  - Lower cost & de-risk technology for long-term sustainable feed-stock



Source: CSIRO.au

### **ASTRI: Establishing a pathway**

- Common path to CST liquid fuels via syngas
  - Leveraging parallel developments in Fischer-Tropsch Liquids (FTL)
- Advance pathway near to long-term feedstock
  - Fossil fuels: Coal and natural gas
  - Low cost biomass: Agricultural residues
  - Future biomass: Micro- and macro-algae
  - Future CO<sub>2</sub>: Thermo-chemical cycles
- Targeted development of selected components
  - Solar hybridised dual fluidised bed (DFB) gasification
  - Super-critical water gasification of algae
  - Reactors for splitting CO<sub>2</sub> and H<sub>2</sub>O into CO
     and H<sub>2</sub>

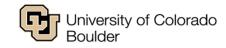






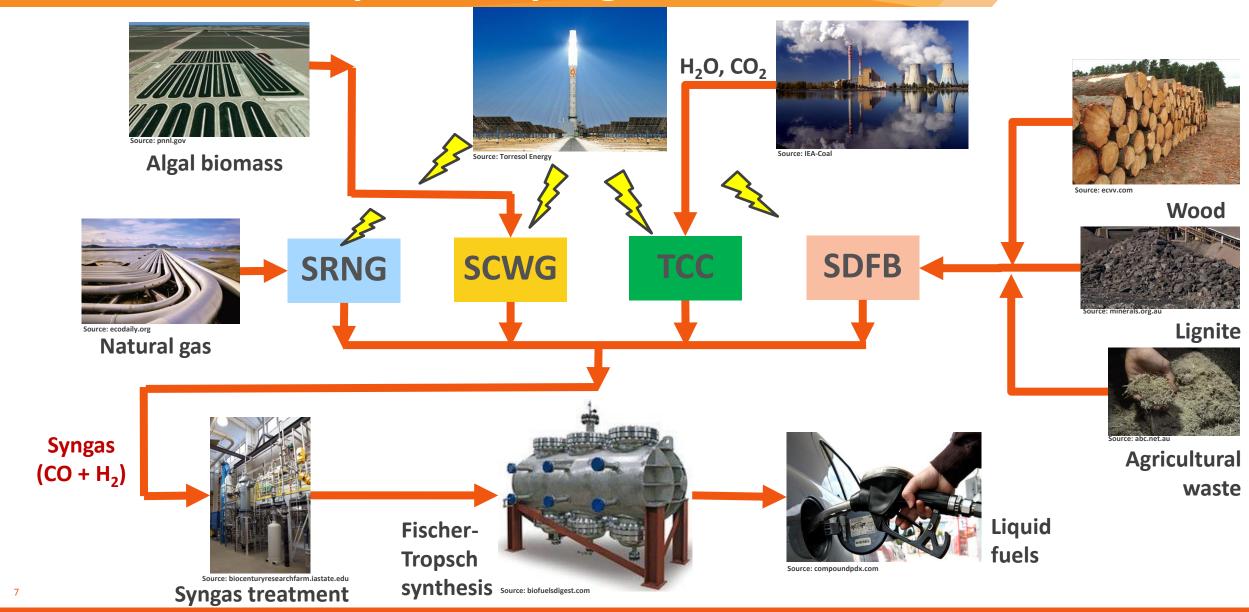








## ASTRI solar-to-liquid-fuel program



## Complementary technologies being developed by ASTRI

Technology	Feed-stock	Temperature	Pressure	Key advantages
Solar hybridised dual fluidised bed gasification	Reactive, dry: Wood, macro-algae, residues, lignite	~ 850 °C	Atmospheric	<ul> <li>Accommodates solar variability upstream of gasifier</li> <li>Heats inert bed material</li> <li>Readily hybridised</li> </ul>
Solar super- critical water gasification	Wet: Micro-algae	~400 – 700 °C	230-250 bar	<ul><li>Low reactor temperature</li><li>Handles wet feed-stock</li><li>No particles in syngas</li></ul>
Thermo- chemical cycles	CO <sub>2</sub> , H <sub>2</sub> O	900 – 1500 °C	Atmospheric	<ul> <li>Realistic path to CO<sub>2</sub> regeneration</li> <li>LCOF \$2.00/L if 25% efficiency can be obtained</li> </ul>
Liquid synthesis catalysts	CO, CO <sub>2</sub> & H <sub>2</sub>	200 – 380 °C	2 – 5 bar	<ul> <li>Higher value products</li> <li>Lower operating temperature</li> <li>More efficient use of precious metal catalysts</li> </ul>

### Distinctive features of ASTRI projects

- Assess whole of plant performance including downstream plant
  - Downstream processing is ~ 45% capex
- Consider solar resource variability in evaluating performance
  - This is a first-order influence
- Establish common framework for techno-economics and LCA CO<sub>2</sub> emissions
  - Compare different technology options for target feed-stock on same basis
- Integrated with, and leveraged from, the other ASTRI projects
  - Heliostats (P11), Receivers (P12) and Energy storage systems (P21)
  - ASTRI 25 100MW scale is well suited to solar fuels
- Integrated national and international program
  - Four Australian and three international institutions







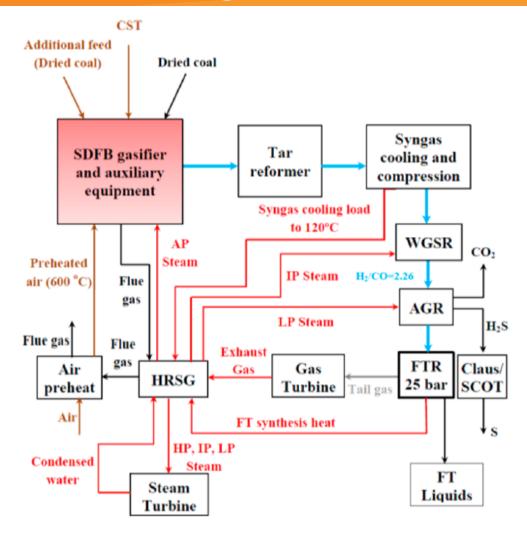






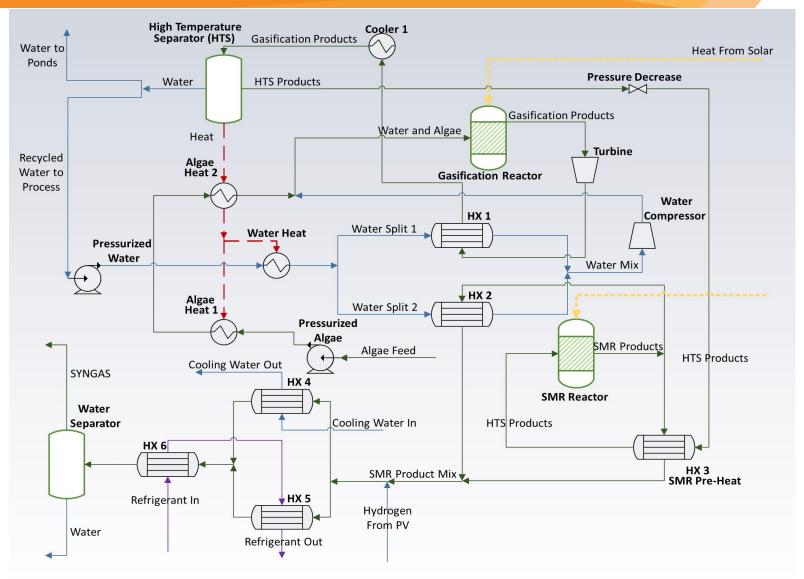


## Modelling the whole process: Here for solar hybridised DFB gasification

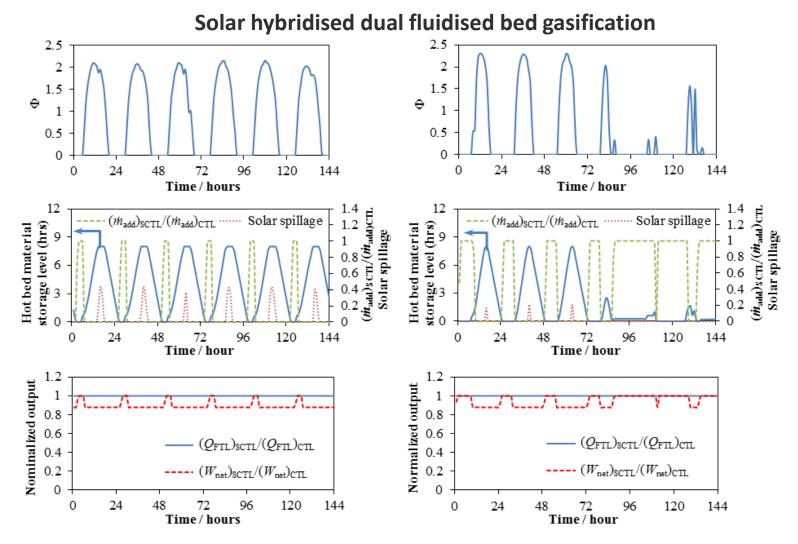


Source: P. Guo, P. J. van Eyk, W. L. Saw, P. J. Ashman, G. J. Nathan and E. B. Stechel, Energy Fuels 2015, 29, 2738-2751

# Process model: Solar super-critical water gasification of algae



## Accounting for solar resource variability six days in 1 year time-series



Source: P. Guo, P. J. van Eyk, W. L. Saw, P. J. Ashman, G. J. Nathan and E. B. Stechel, Energy Fuels 2015, 29, 2738-2751

## **Levelised cost of fuel (LCOF) – Year 2020**

Low sulphur diesel (LSD) Australian Institute of Petroleum

LSD \$1.1/L (TGPb)

Short-term Solar mixed reforming of natural gas (CSIRO) 3 CH<sub>4</sub> + 2 H<sub>2</sub>O + CO<sub>2</sub>

**Diesel/Gasoline** < 750°C (1-15 bar) -Catalyst + FTS \$1.0/L

Solar hybridised gasification of coal + CCS (UA/ASU/ETH)  $C + H_2O$ 

Diesel/Gasoline SDFB - 850°C (1 bar) + Syngas upgrading + \$0.9/L

Solar hybridised gasification of biomass (UA/ASU/ETH)  $C + H_2O$ 

Diesel/Gasoline SDFB - 850°C (1 bar) + Syngas upgrading + FTS \$1.4/L

Solar SCWG of microalgae (ANU/UC/UA)  $C_aH_bO_cN_d \bullet (H_2O)$ 

400-700°C (230-250 bar) with catalyst + Syngas upgrading + FTS

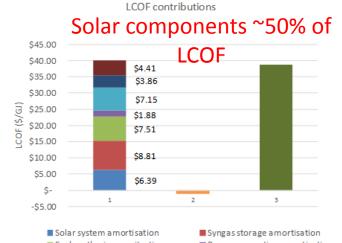
TC cycles to split H<sub>2</sub>O + CO<sub>2</sub> (ANU/CSIRO)  $CO_2 + 2 H_2O$ 

900-1500°C (1 bar) - Metal oxides (non-stoic.)

Diesel/Gasoline \$2.0/L

Input fuel cost

a- Mui, S., Tonachel, L., McEnaney, B. and Shope, E., GHG Emission Factors for High Carbon Intensity Crude Oils. Natural Resources Defense Council, 2010. b- http://www.aip.com.au/October 2015, Terminal Gate Price



■ Fuel synthesis amoritsation ■ Power generation amortisation

■ Electricity sales offset

■ O&M solar system ■ O&M fuel synthesis ■ TOTAL LCOP

E.g. Distribution of LCOF contributions for SRNG

Diesel/Gasoline \$3.0/L



**CSIRO** 

THE UNIVERSITY

of ADELAIDE

Australian

University

National



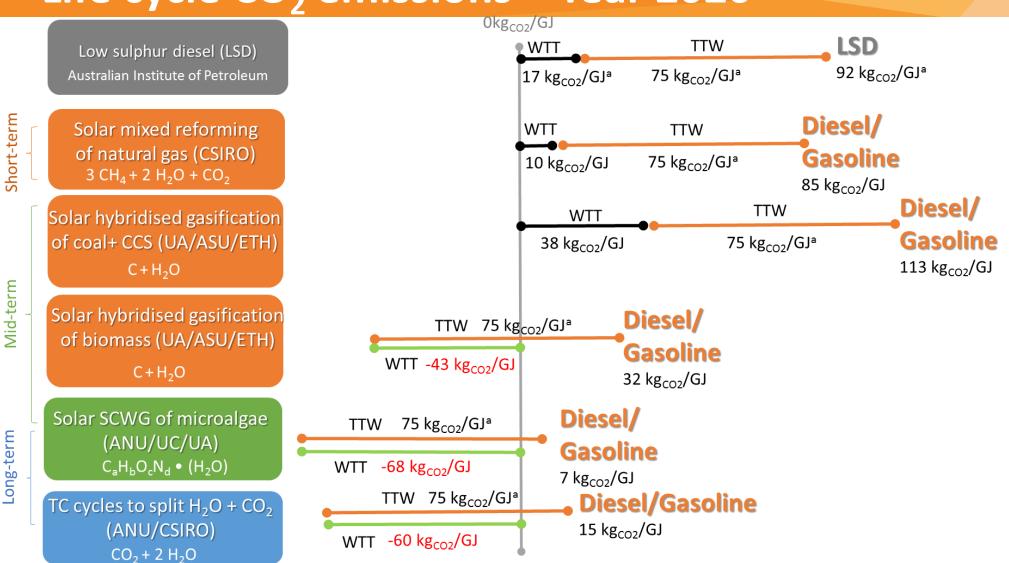




Mid-term

ong-term

## Life cycle CO<sub>2</sub> emissions – Year 2020

















### **Current status of assessment matrix**

Process	Technical feasibility (22%)	Solar share (10%)	Economic feasibility (33%)	Sustainability (20%)	Stage of development (15%)	Overall	Priority
Solar mixed reforming of methane	7.8	3.0	6.8	2.5	6.5	5.7	1
Solar hybridized coal gasification via vortex flow reactor	6.3	3.0	5.3	1.0	4.5	4.3	2
Solar hybridized coal gasification via dual fluidised bed gasifier	7.5	3.0	7.1	1.0	6.0	5.4	1
Solar hybridized biomass gasification via dual fluidised bed gasifier	7.0	3.0	4.5	9.0	6.0	6.0	1
Supercritical water gasification of Algae	5.8	5.0	2.3	9.0	6.5	5.3	1
Thermochemical cycles	5.0	10.0	2.3	7.8	7.0	5.4	1















## Technology development: Solar hybridised DFB gasification (UA/ASU/ETH)

An economic process that delivers a constant production rate of liquid fuels despite solar variability

#### Leverages existing/parallel technology:

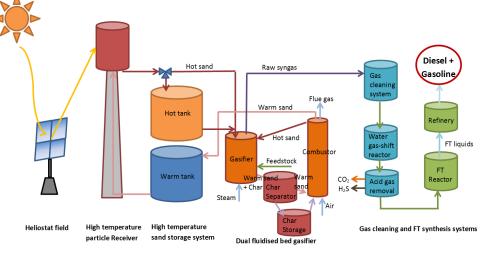
- Fluidised bed gasification technology has been demonstrated
- Other ASTRI projects

#### New understanding for target feedstocks/bed material:

- Bed material (physical/thermal/catalytic properties)
- Torrefaction of agricultural residues and algae
- Char reactivity of biomass under gasification environment
- Increases viability for gasification

#### **Future research activities:**

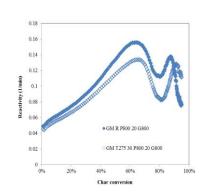
- Interaction between solar radiation and fuel ash/bed material
- Planning toward pilot-scale testing



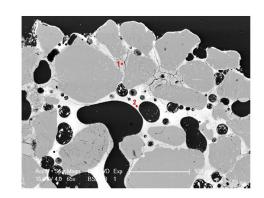
P11 P12 P21

P42 Co

Commercially available

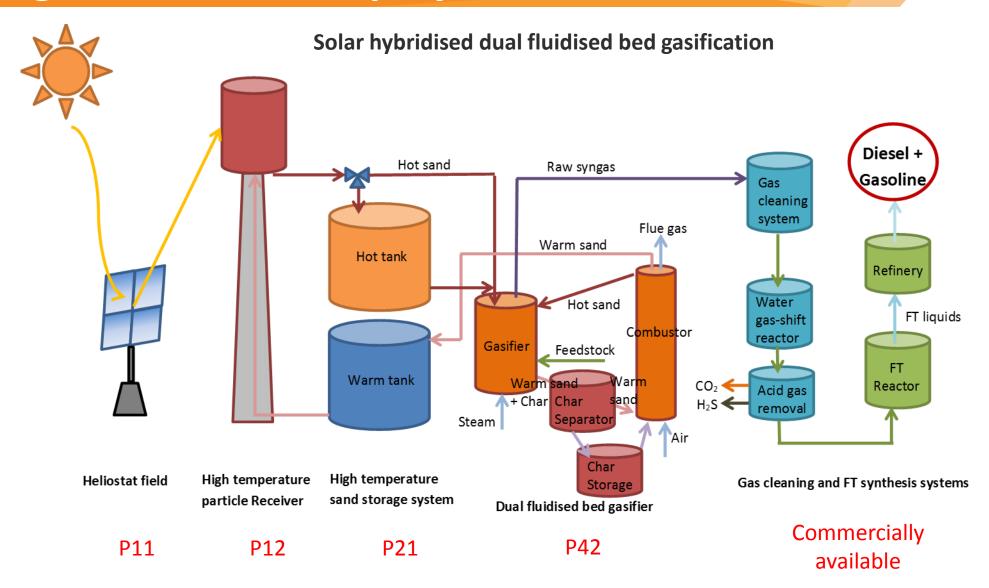


Char reactivity-Grape marc



Cross section of an agglomerate

### Linkages across ASTRI projects



# Technology development: Solar SCWG (ANU/UC/UA)

#### Leverages existing/parallel technology:

- H<sub>2</sub> and CH<sub>4</sub> as targets, not liquid fuels
- Leverages understanding of tubular receivers from P12

#### New understanding for reactor/target feedstock:

- Reaction kinetics for micro-algae under SCWG
- Heat and mass transfer of the reactor

#### Provision of new design data:

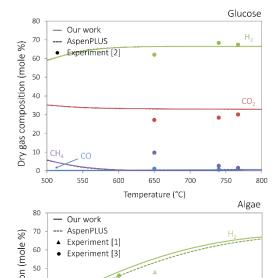
- Materials selection, stress analysis
- System integration

#### **Future research activities:**

- Experimental/modelling assessment of transients
- Detailed techno-economic assessment
- Planning toward pilot-scale testing



New rig under construction



Developing validated models of reactions

## Technology development: Thermo-chemical cycles (ANU/CSIRO)

#### **Complements international R&D:**

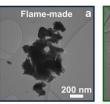
- Through novel nano-structured metal oxides
  - $\triangleright$  Efficient redox material with improved  $\delta/\Delta T/P_{O2}$

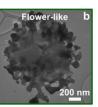
#### **Novel reactor development:**

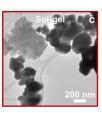
- Reduce radiation losses
- Increase heat recovery

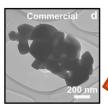
#### **Future research activities:**

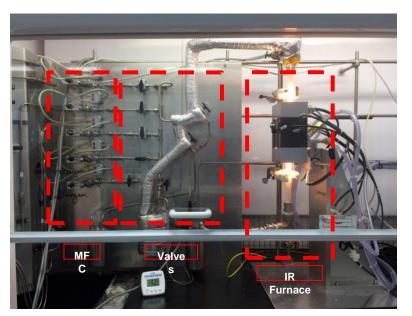
- Further development of Red-Ox materials
- Testing of reactor with Red-Ox materials
- Planning toward pilot-scale testing



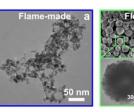


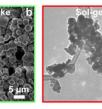


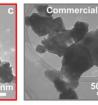












## Technology development: Advanced Sabatier (UA/Flinders)

#### **Complements international R&D:**

- Demonstrated use of novel metal cluster catalysts deposited on titania (TiO<sub>2</sub>)
  - Very efficient use of every metal atom

#### **Reactor development:**

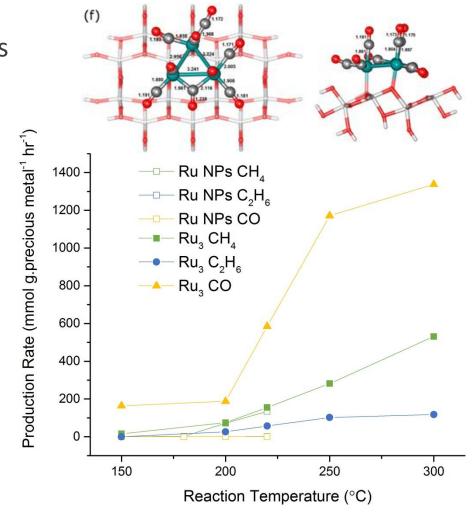
- Small cell volume reactors
- Batch and continuous flow

#### **Calculations:**

- Cluster allows for exact calculations
- Identified energy of ligand removal

#### **Future research activities:**

- Further testing of other clusters
- Reactivity calculations
- Optimising for longer hydrocarbons



Ru<sub>3</sub> cluster vs RuNPs on anatase, rxn at 250 °C

## **Concluding comments (1)**

- Sustainable liquid fuels: Important component of Australia's future energy mix (& global)
  - Vital in air-transport, important in heavy freight, agriculture, mining, hybrid vehicles
- ASTRI has established a common-platform for comparing different technology pathways
  - Identified technologies with realistic potential for \$0.8/L < LCOE < \$1.4/L</li>
  - Plan to broaden framework into common international platform
- CST expected to play a vital role in the lowest cost path to sustainable fuels
  - Biomass co-products: CST increases output by ~ 30-40% of lowest cost, limited resource
  - Algal feed-stock: CST expected to lower cost of "Gen III bio-fuels" to form "bio-solar-fuels"
  - CO<sub>2</sub> feed-stock: CST offers plausible path to CO<sub>2</sub> regeneration, which may be necessary
- ASTRI is driving low-cost technology development for each core feed-stock
  - Solar hybridised DFB gasification: Novel platform with low technical risk, suits biomass co-products
  - Solar super-critical gasification: Well suited to wet feed-stock (micro-algae) novel path to lower cost
  - CO<sub>2</sub> Regeneration: Targeting novel materials and reactors to lower the cost in the longer-term

## **Future plans**

- Expand international partnerships to better coordinate efforts
  - Expand common platform to allow cross comparison of different feed-stocks and technologies
  - Explore benefit of complementary components in a system
- Expand industry partnership
  - End-users, including agricultural and mining sectors
  - Technology providers, including CST, feed-stock providers, fuels processors
- Drive high value technology options through scale-up and development
  - Access international facilities for scale-up
  - Using international partnerships to attract additional resources

## Acknowledgements





#### **Australian Government**

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## Thank you

#### **Market Barriers**

- Higher capital cost of syngas processing plant
  - Cost depends on solar reactor performance
  - Costs sensitive to intermittent operation
  - Economics challenging to estimate
- Solar fuels reactors are pre-commercial
  - Reactor design sensitive to feed-stock
- Need a path-way to market
  - Establish with high value, niche products
  - Develop capacity for long-term feed-stock



Source: CSIRO.au