



## ASTRI Solar Fuels Preliminary Study to set LCOF Benchmark ASTRI Annual Workshop, 2015

G. Nathan<sup>1</sup>, P. Ashman<sup>1</sup>, W. Saw<sup>1</sup>, P. van Eyk<sup>1</sup>, P. Guo<sup>1</sup>, G. Metha<sup>1</sup>, J. Alvino<sup>1</sup>, C. Doonan<sup>1</sup>, D. Losic<sup>1</sup>, R. Karunagaran<sup>1</sup>, A. Bayon<sup>2</sup>, J. Hinkley<sup>2</sup>, J. Pye<sup>3</sup>, W. Lipinskí<sup>3</sup>, M. Venkataraman<sup>3</sup>, A. Weimer<sup>3,4</sup>, T. Nann<sup>5</sup>, G. Andersson<sup>6</sup>, E. Stechel<sup>7</sup>, A. Steinfeld<sup>8</sup>

<sup>1</sup>The University of Adelaide <sup>2</sup>CSIRO <sup>3</sup>Australian National University <sup>4</sup>University of Colorado <sup>5</sup>Flinders University <sup>6</sup>University of South Australia <sup>7</sup>Arizona State University <sup>8</sup>ETH Zürich

11<sup>th</sup> February 2015

#### Background

#### Need for Targets for cost and broad viability

#### • IEA's Solar PACES Executive committee identified (at last meeting):

- Cost targets are needed to drive development of solar chemistry
  - None are available to our knowledge

#### Setting realistic targets is challenging because

- Solar chemistry is at a much earlier stage of development than solar power
  - No commercial plants have been built
  - > No pilot-scale plants have been built of the full process
- Significant differences between commercial and solar chemical process
  - > Commercial processes are steady while the solar resource is intermittent
  - Commercial processes are 10 1,000 times larger
- Significant differences between CST power and chemical process
  - > Chemical plants operate at higher temperature than current power plants
  - > Solar reactors typically differ from solar receivers
  - > Solar chemistry are typically more complex, with more downstream processing
- The diversity of chemical process is greater than for power plants
  - Many types of fuels and mineral processes
  - Many options within each type of chemical process
  - No standardised methodology with which to compare different options

#### Background **Conventional and Solar Gasification (and reforming)**

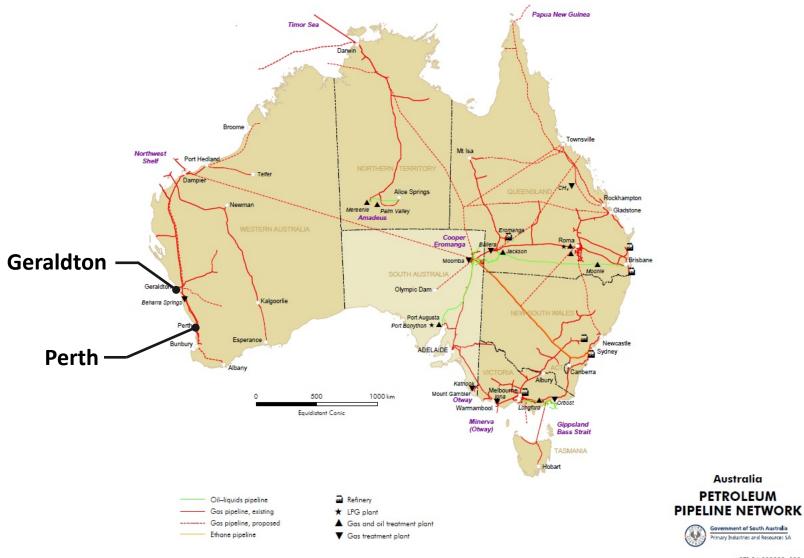
#### **Solar Gasification** 02 Coal + CO<sub>2</sub> + Heat Coal and/or **Biomass** СО Processing Gasification $H_2$ Plant $H_2O$ Diesel

#### **Conventional Gasification**

## **ASTRI Approach**

- Selected Solar Fuels as the process closest to commercial
  - 1<sup>st</sup> Aust. Workshop on Solar Thermal Chemical Processes, Adel. Jan. 2013
  - Syngas production has been demonstrated at 250 kW
  - Long-term commercial drivers for fuels as high value product
- Developed a set of standard conditions by expert opinion
  - Solar Receiver Scale: 50 MW thermal
  - FT (mini) reactor scale: 1500 bbl/day (9.94m<sup>3</sup>/h)
- Selected Reference site as Geraldton, WA
  - good solar resource, 6.6 kWh/m<sup>2</sup>/day (DNI)
  - Ready access to all feedstocks (natural gas, coal, wood)
  - Access to seawater for growing algae (micro / macro)
- Selected common economic parameters

#### **ASTRI Reference Location**



## **ASTRI Reference Field Design**



#### **Field Design**

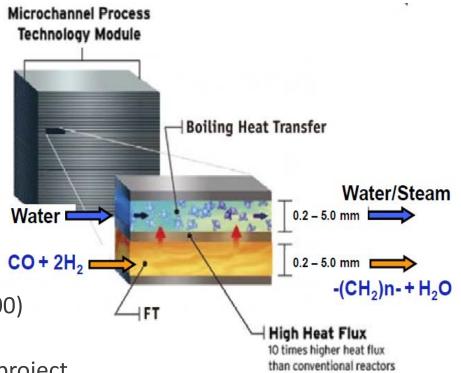
Developed with SAM Scaled down from: 270 MW<sub>th</sub> = 100 MW<sub>e</sub>

PARAMETER	CAVITY RECEIVER	EXTERNAL RECEIVER
Type of field	Sector	Surround
Design thermal incident power, MW <sub>th</sub>	270.6	270.6
Tower height (100 MW <sub>e</sub> ), m	133	223
Solar multiple	1.33	1.33
Field size (100 MW $_{ m e}$ ), m $^2$	708,933	748,104
Optical efficiency of solar field <sup>‡</sup>	56.4%	53.5%
Approximate field size, 50 MW <sub>th</sub>	130,999	138,237

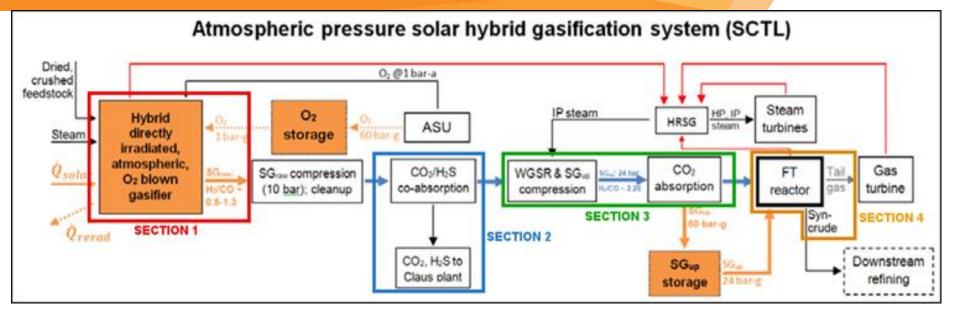
DESIGN POINT RADIATION TO RECEIVER	50,000	KW
Design point DNI	900	W/m <sup>2</sup>
Annual energy yield	110.5	MWh
Solar field capacity factor (annual)	28.9%	
Solar field optical efficiency at design point	58.8%	

## **Turn-down of FT-reactor**

- Current FT Reactors:
  - Employ large tubes
  - Take > 5 days to stabilise
  - No turn-down capability
- New mini-micro reactors
  - Employ small channels or tubes
  - $\sim$  10  $\times$  higher rates of heat transfer
  - Economic at much smaller scale (< 1/100)
  - Have potential for large turn-down
    - > Being assessed within current ASTRI project
- Various approaches adopted in preliminary assessment
  - Three Hybrid processes: all achieve continuous production
  - Methane reforming: Storage 61% average daily output (requires turn-down)
  - Super-critical gasification: 6 hours storage (requires turn-down)



#### **ASTRI Process modelling**



- Processes models were developed for each technology option
  - All assumed "pseudo-steady-state" steady at each time-step
  - Accounted for resource variability, but in different ways
    - > Hybrid cases ensured full output was maintained throughout year

#### **ASTRI – Key economic parameters**

$$LCOF = \frac{\sum_{t=1}^{n} (I_t + M_t + F_t - S_t)/(1+r)^t}{\sum_{t=1}^{n} (E_t)/(1+r)^t}$$

LCOF = Levelised cost of fuel in \$/GJ (\$/Litre)

- $I_t$  = Investment expenditure or capital cost in the year t
- $M_t$  = Operations and maintenance cost in the year t
- $F_t$  = Feedstock cost in the year t
- $S_t$  = Annual sale price of any electricity in the year *t*, if produced from the process, in AUD
- $E_t$  = Quantity of energy produced (GJ), including electricity for sale in year *t*.
- r = Discount rate
- *n* = Amortisation period

# **ASTRI – Key economic parameters**

SOLAR COST COMPONENTS	CURRENT COST (2014 AUD)	FUTURE COST 2020 (2014 AUD)	UNITS		
Solar Field plus site costs	240	135	\$/m²		
Tower	51.0	46.6	\$/kW <sub>th</sub>		
Receiver (based on molten salt)	150.8	137.7	\$/kW <sub>th</sub>		
BOP solar	35.1	32.1	\$/kW <sub>th</sub>		
Solar field O&M	65	55.8	\$/(kW <sub>th</sub> .year)		
Power generation	1025	965	\$/kW <sub>e</sub>		
Syngas storage	20,833	19,027	\$/GJ		

## **ASTRI – Summary of economic analysis**

Process	Technical feasibility (22%)	Solar share (10%)	Economic feasibility	-LCOF (\$/L)	Sustainability (20%)	-Feedstock sustainability · · · · · · · · · · · ·	-CO <sub>2</sub> emission (50%)	Stage of development (15%)	Overall	Priority
Solar mixed reforming of methane	7.8	3.0	6.8	\$1.0/L	2.5	1.0	4.0	6.5	5.7	1
Solar hybridized coal gasification via vortex flow reactor	6.3	3.0	5.3	\$1.2/L	1.0	1.0	1.0	4.5	4.3	2
Solar hybridized coal gasification via dual fluidised bed gasifier	7.5	3.0	7.1	\$0.9/L	1.0	1.0	1.0	6.0	5.4	1
Solar hybridized biomass gasification via dual fluidised bed gasifier	7.0	3.0	4.5	\$1.4/L	9.0	8.0	10.0	6.0	6.0	1
Supercritical water gasification of Algae	5.8	5.0	2.3	\$2.9/L	9.0	8.0	10.0	6.5	5.3	1
Thermochemical cycles	5.0	10.0	2.3	\$2.0/L	7.8	5.5	10.0	7.0	5.4	1

- ASTRI Milestones for costs by Dec 2016:
  - \$1.20/L for fossil fuel feedstock with a life-cycle emission of CO<sub>2</sub> that is at least 10% lower than conventional diesel, and
  - 2.50/L for future renewable feedstock with a life-cycle emission of CO<sub>2</sub> that is at least 50% lower than conventional diesel.
    - Note: "Targets" could be set lower
- ASTRI milestone for wholistic viability:

develop a broad assessment system

# Acknowledgements



The Australian Solar Thermal Research Initiative (ASTRI) Program is supported by the Australian Government through the Australian Renewable Energy Agency (ARENA).













# Thank you

